

## ULTRASONIC METHOD TO DETERMINE THE PHENOMENA INSIDE A CONTINUOUS CHANGING SYSTEM

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**Abstract.** This work studies the way in which ultrasonic waves can detect the development of a continuous changing system, knowing that wave propagation is non-destructive and does not modify with the crossed system. These changes influence a lot the measurable parameters of ultrasounds. The variation of both velocity and attenuation coefficient were studied during ultrasounds propagation, while crossing a system which passes from liquid to gel. As an application for this phenomenon, the optimum conditions for milk coagulation were determined; this is very important in food industry. Ultrasounds velocity and attenuation measurements were made depending on the temperature (15<sup>0</sup>C, 25<sup>0</sup>C, 35<sup>0</sup>C) and concentration of CaCl<sub>2</sub> solution 40% added to the system (0.10g/l, 0.15g/l, 0.12g/l).

*Key words:* Ultrasound, Velocity, Attenuation coefficient, Coagulation, Gel.

### 1. INTRODUCTION AND THEORY

Ultrasounds reflect on any discontinuity, which exists in an environment, leading to differences of measurable parameters. [7]

The scalar wave equation, that governs wave propagation phenomena in ideal liquids, is given by:

$$\frac{\partial^2 \psi}{\partial t^2} = v^2 \left( \frac{\partial^2 \psi}{\partial x^2} + \frac{\partial^2 \psi}{\partial y^2} + \frac{\partial^2 \psi}{\partial z^2} \right) = v^2 \Delta \psi \quad (1)$$

where:  $\psi$  is the wave function, usually describing displacements and  $v$  is propagation velocity.

Only longitudinal waves propagate in fluids. Their propagation velocity  $v_l$  is given by:

$$v_l^2 = 1/\rho\beta \quad (2)$$

where  $\beta$  is the compressing coefficient given by  $\beta = 1/\gamma p$  ( $\gamma$  adiabatic coefficient,  $p$  pressure) and  $\rho$  density.

But not all the liquids can be approximated as ideal. In these liquids, attenuation phenomena must be taken into account. The attenuation coefficient ( $\alpha$ ) is a sum between the absorption coefficient ( $\alpha_a$ ) which is proportional with the wave frequency and does not depend on the scattered size in the environment and the dispersion coefficient ( $\alpha_d$ ), or scatter coefficient, which depends on frequency and also on the size of the scatterings:

$$\alpha = \alpha_a + \alpha_d \quad (3)$$

The  $\alpha$  coefficient depends on the nature of the environment, but also on the wave type or wave length, but it can be considered, as a first approximation, as constant for an environment and for a wave with given characteristics.

If the relaxation is neglected, the absorption coefficient is:

$$\alpha_a = \frac{\omega^2 \tau}{2v(1 + \omega^2 \tau^2)} \quad (4)$$

where:  $\omega$  is pulsation,  $\tau$  is relaxation time and  $v$  is the wave propagation velocity.

If the wave frequency is much lower then the relaxation frequency  $\omega^2\tau^2 \ll 1$ , the attenuation constant will be:

$$\alpha_a = \frac{\omega^2 \tau}{2v} \quad (5)$$

In the case of very low density, the absorption coefficient is regarded as a sum of parameters given by separate phenomena, as viscosity, conductivity and radiation:

$$\alpha = \alpha_{visc} + \alpha_{cond} + \alpha_{rad} \quad (6)$$

where:

$$\alpha_{visc} = \frac{8}{3} \frac{\pi^2 f^2 \eta}{\rho v^3} \quad (7)$$

$$\alpha_{cond} = \left( \frac{\chi-1}{\chi} \right) \frac{q}{2v} \quad (8)$$

where:  $f$  is the wave frequency,  $\eta$  is viscosity,  $\chi$  is the conductivity coefficient and  $q$  is given by Newton's law:

$$T-T_l = (T_0-T_l) \cdot e^{-qt} \quad (9)$$

where:  $(T-T_l)$  is the temperature excess at the  $t$  moment and  $(T_0-T_l)$  is the temperature excess at the moment  $t_0$ .

Practically only the first two parameters in equation (6) are taken in consideration for the linear processes.

For high frequencies, when the wave length is much higher than the scatterers diameter ( $\lambda \ll d$ ), the attenuation takes place on each scatterer, and the attenuation coefficient is proportional with the square frequency.

If  $\lambda \cong d$ , the ultrasounds are attenuated by the interferences of different scatterers and the attenuation is mainly given by the absorption processes.

When  $\lambda \gg d$ , the ultrasounds are diffused by small particles which form the propagation environment and the attenuation is given by the thermal conduction, case in which the attenuation coefficient is proportional with biquadrate frequency [11].

It can be said that the size of the attenuation coefficient can give information regarding the physical characteristics of the environment, which leads to a development of new ultrasounds measuring, and control methods.

This work refers to an ultrasonic method to observe the gel formation with the application in the milk coagulation process, bound for the milk industry, the research laboratories from this field, etc.

This phenomenon is the result of casein limited proteolysis. The chymosine action develops in two stages: the first stage is enzymatic and the second is coagulation. In the second stage, only after the physico-chemical transformations of the micelles, which lead to the formation of a three-dimensional network, the aggregation begins [2], [4], [8], [9].

In the purpose of determining the final moment of milk coagulation some methods are known:

- visual observation method, which consists in taking of samples and in establishing with the naked eye the coagulation moment; this method depends on the visual capacity of the person who makes the determinations, so, it is extremely subjective [1], [3], [10].
- physical methods (electronic scanning, viscosity determination and electrocynetical phenomena, particles counting, optical methods); these methods imply a long time of study, during which the system changes, they cannot be adapted on line in the technological flow so, the results have distortions sometimes [5], [6].

- viscoelastimetical and manometrical methods, which permit observing of the evolution of the system reological properties by taking of samples; by using these methods, the results are different (they depend on authors and on techniques used) because they are expressed in arbitrary units [10], [12].

Ultrasonic methods eliminate these disadvantages because it permits the establishing, with accuracy, of the final moment of milk coagulation - this moment being very important for the milk products quality [8].

## 2. MATERIAL AND METHODS

This method is based on the measurements, with an ultrasonic installation (Fig. 1), of ultrasonic parameters: ultrasonic velocity- $v$ (m/s) and attenuation coefficient- $\alpha$ (dB/m), during their propagation through the milk: the transducer (2) is mounted on the tank's wall (1), which is connected to the flaw detector (4) with a coaxial cable (3). On the screen (5) all the ultrasonic interest parameters can be read. From the interpretation of these values, it is possible to determine all of the phases of the milk coagulation. Next, it will be observed the variation of velocity and attenuation coefficient of ultrasonic waves during the milk coagulation process [10].

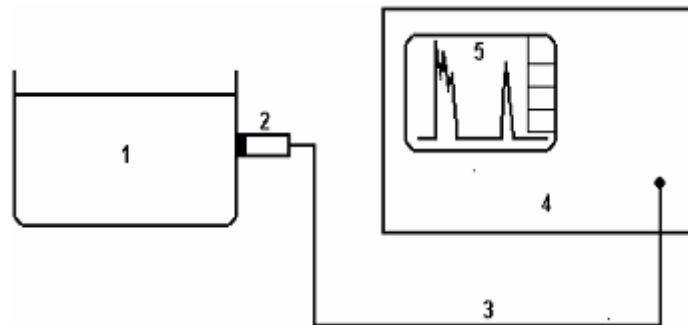


Fig. 1 Experimental set-up for ultrasonic velocity and attenuation coefficient determination for oversee the milk coagulation process

## 3. RESULTS

### 3.1 Influence of the temperature on the milk coagulation process

In the experiments 5ml pepsin solution 1% in 250ml of milk are used. For each sample, the 0.20g/l of 40%  $\text{CaCl}_2$  solution is added. The ultrasonic velocity (Fig. 2) and attenuation coefficient (Fig. 3) are measured at 15°C, 25°C and 35°C.

The ultrasonic velocity is bigger for the milk coagulation at the  $T=35^\circ\text{C}$  (Fig. 2). The slope of the curve is bigger in the first minutes. This fact indicates the aggregate formation – distinctive phenomenon of the gel. In the first 30s, the system does not suffer important modifications ( $\delta(\Delta v) = 3\text{m/s}$ ). In this first stage, only one fraction of the casein molecule is hydrolyzed, so the phenomenon begins after 30s. After this moment, the ultrasonic velocity begins to increase, this indicates that the system begins the transformations and the first micelles appear. The transformations continue on the 7min period therefore in this period the coagulation process occurs. From the 8 min, the velocity variation is abrupt, thus in only one minute, the ultrasonic velocity increases with 15,5m/s. This lead out of one's initial curve is associated with the first contraction of the three-dimensional network apparition. This phenomenon precedes the beginning of syneresis.

The attenuation coefficient has an important increase during the whole period of the micelles apparition (Fig. 3). This behaviour is in a concordance with the phenomenon of transforming the fluid state into the gel state. The abrupt decreasing of the attenuation coefficient coincides with the increasing of the ultrasonic velocity, therefore the modification of the system structure is pointed out.

For the 25°C and 15°C temperatures, the ultrasonic velocity increases very slowly ( $\delta(\Delta v) = 25,4\text{m/s}$ , respectively  $\delta(\Delta v) = 11,1\text{m/s}$  in 10min). Also, the variation of the attenuation coefficient is less significant ( $\delta(\Delta\alpha) = 1,16\text{dB/m}$ , respectively  $\delta(\Delta\alpha) = 0,23\text{dB/m}$  in 10min), therefore it is confirmed the fact that the system has not modified its structure. In conclusion, Table 1 presents the time of the apparition of the first micelles.

$T$ (°C)	$t$ (min)
15	2
25	1.5
35	0.5

Solution 40% CaCl <sub>2</sub> (g/l)	$t$ (min)
0.10	4
0.15	1
0.20	0.5

### 3.2 Influence of CaCl<sub>2</sub> concentration on the milk coagulation process

In the experiments 5ml pepsin solution 1% in 250ml of milk are used. The temperature of the samples is constant  $T=35^\circ\text{C}$ . The ultrasonic velocity (Fig. 4) and attenuation coefficient (Fig. 5) for the different quantities (0.10g/l, 0.15g/l and 0.20g/l) of 40% CaCl<sub>2</sub> solution are measured. From Fig. 4 it can be observed that the ultrasonic velocity is bigger during the milk coagulation with the add of 0.20g/l CaCl<sub>2</sub> solution concentration, compared to the samples with 0.15g/l and 0.10g/l CaCl<sub>2</sub> solutions.

If for the sample with 0.20g/l CaCl<sub>2</sub> solution, the velocity attains a bearing after 6min (therefore the system attains an equilibrium), for the sample with 0.15g/l and respectively 0.10g/l CaCl<sub>2</sub> solution, the variations are  $\delta(\Delta v) = 41\text{m/s}$ , respectively  $\delta(\Delta v) = 14\text{m/s}$  in 10min, that is the merely the beginning of the micelles formation. The same conclusions derive also from the variation of the attenuation coefficient (Fig. 5). In conclusion, Table 2 presents the time for the first micelles apparition.

## 4. CONCLUSIONS

The ultrasonic propagation through the system is influenced by its state, therefore the ultrasonic parameters (ultrasonic velocity and attenuation coefficient) are in direct relation with the gel formation. Until the beginning of milk coagulation, the ultrasonic velocity is constant.

With the appearance of the first micelles, the ultrasonic velocity increases. This increasing is important until the system attain an equilibrium that is until the gel's three-dimensional network becomes stable. The constant ultrasonic velocity observes this fact. This indicates the end of the milk coagulation.

After these two essential stages, other two phenomena can be observed owed to the coagulant enzymes: the stage of general proteolysis and the syneresis stage (which is a physico-chemical phenomenon that manifests by the contraction of the gel and by the whey elimination).

The syneresis phenomenon is also observed by the sudden decrease of the attenuation coefficient, after the velocity attains a bearing. This behaviour is due to the apparition of two phases: the gel phase and the liquid phase, which determine the ultrasonic velocity modification.

During the coagulation period, the ultrasonic absorption increases because of the liquid mechanical modulus increase. The attenuation coefficient increases proportionally with the shape, the size and the number of the micelles, because the main factor of the attenuation is the scatters.

This method is very precise and rapid, excludes the subjectivism, and does not determine the denaturation phenomena of the examined product. In this case it is not necessary the taking of the samples during the whole process period.

This method is not noxious for the staff that accomplishes the determinations and may be adapted on line in the technological flow.

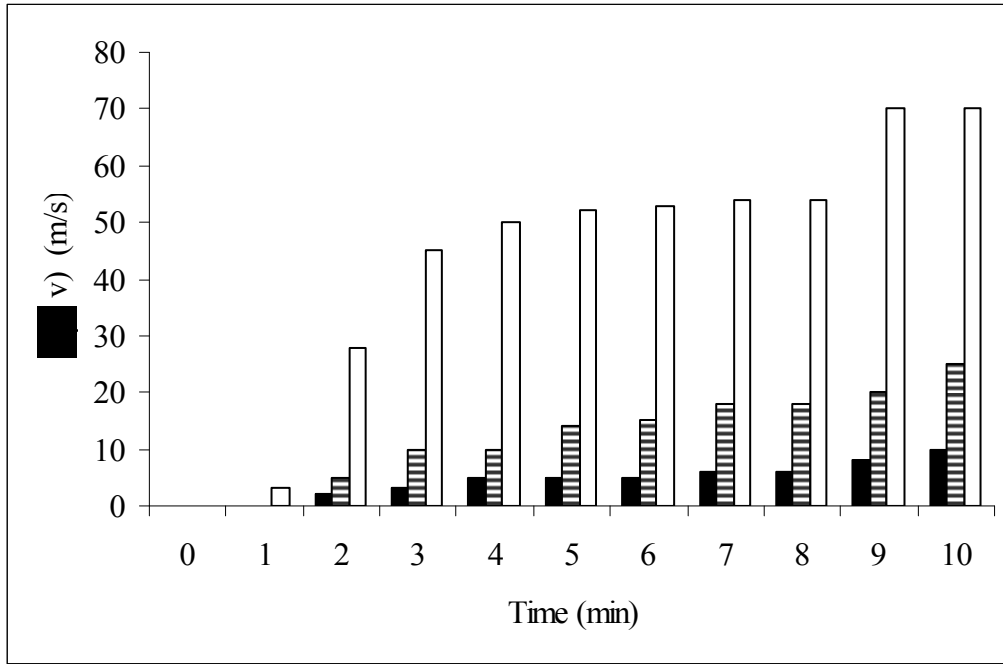


Fig.2 Variation of ultrasonic velocity with time and temperature for milk with 0.20g/l of 40% CaCl<sub>2</sub> solution  
 (■) T=15<sup>0</sup>C; (≡) T=25<sup>0</sup>C; (□) T=35<sup>0</sup>C.

For T=35<sup>0</sup>C, the dependence of ultrasonic velocity *versus* time is gives by:  
 $\delta(\Delta v)(t) = 0.1704 t^3 - 3.8065t^2 + 30.766t - 33.409$  (where R<sup>2</sup> = 0.9497)

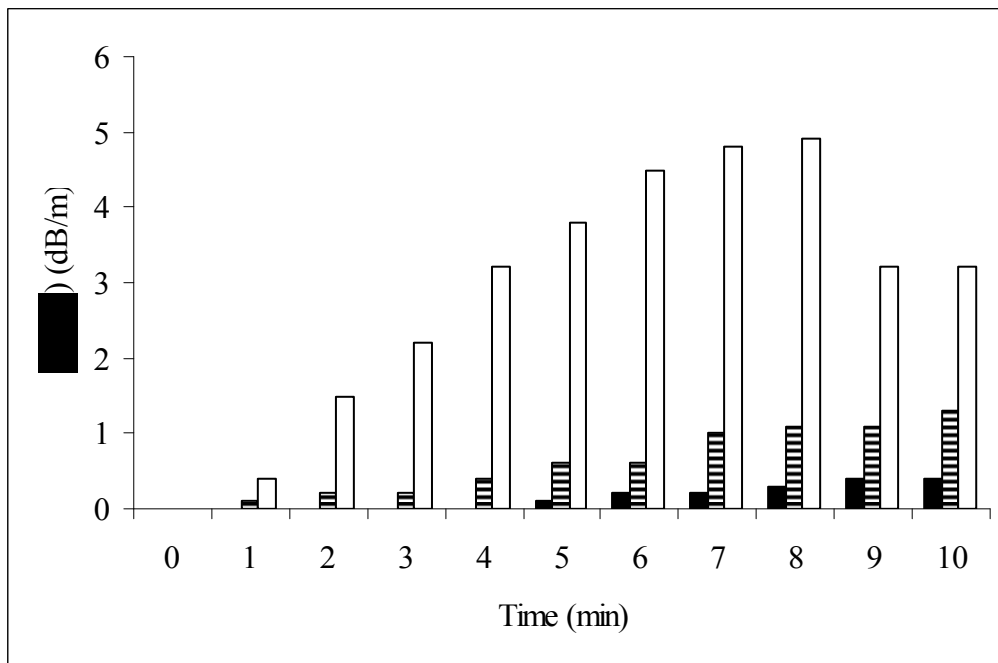


Fig. 3 Variation of attenuation coefficient with time and temperature for milk with 0.20g/l of 40% CaCl<sub>2</sub> solution  
 (■) T=15<sup>0</sup>C; (≡) T=25<sup>0</sup>C; (□) T=35<sup>0</sup>C.

For T=35<sup>0</sup>C, the dependence of attenuation coefficient *versus* time is gives by:  
 $\delta(\Delta \alpha)(t) = -0.0143t^3 + 0.157t^2 + 0.3137t - 0.5606$  (where R<sup>2</sup> = 0.9671)

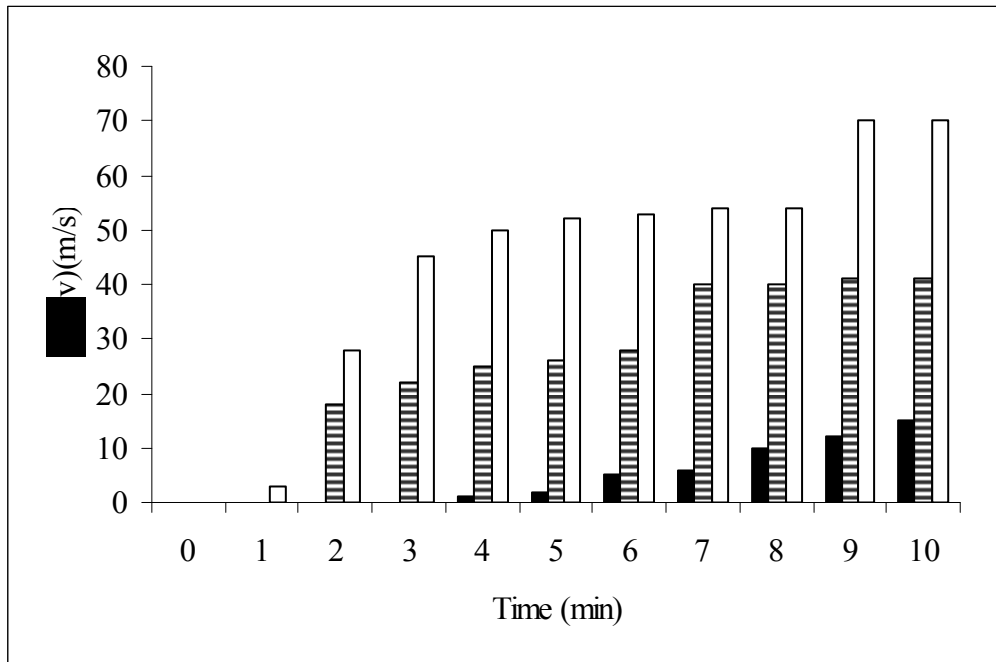


Fig. 4 Variation of ultrasonic velocity with time and quantity of solution 40%  $\text{CaCl}_2$  in milk at  $T=35^\circ\text{C}$ . (■)  $c=0.10\text{g/l}$ ; (≡)  $c=0.15\text{g/l}$ ; (□)  $c=0.20\text{g/l}$ .

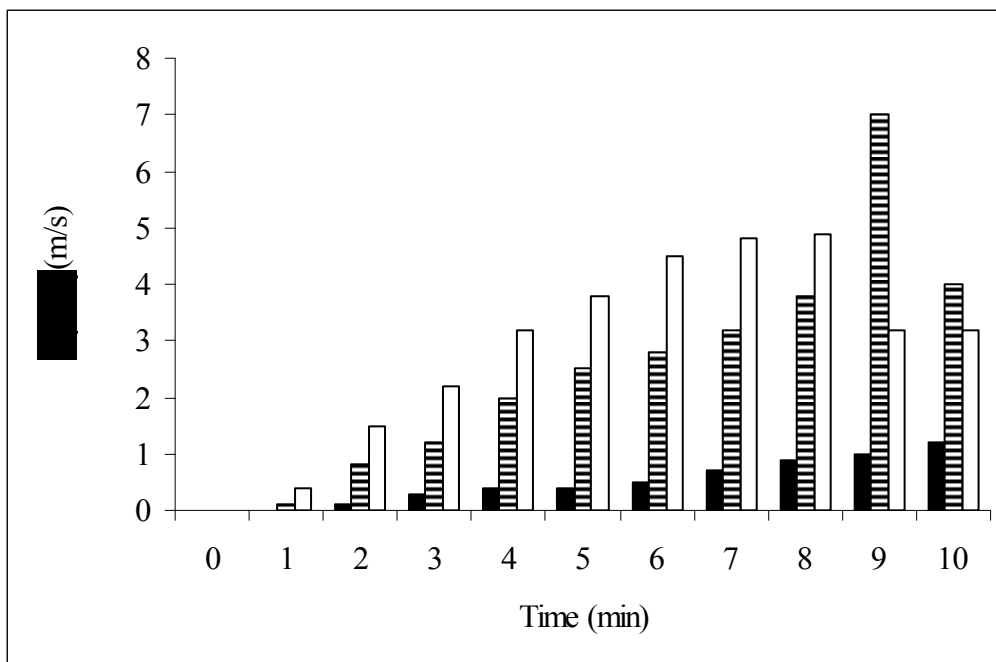


Fig. 5 Variation of attenuation coefficient with time and quantity of solution 40%  $\text{CaCl}_2$  in milk at  $T=35^\circ\text{C}$ . (■)  $c=0.10\text{g/l}$ ; (≡)  $c=0.15\text{g/l}$ ; (□)  $c=0.20\text{g/l}$ .

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